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**MFIX Phi** 

**MFIX-DEM Phi: Performance and Capability Improvements  
Towards Industrial Grade Open-source DEM Framework with  
Integrated Uncertainty Quantification**

M. Adepu, S. Chen  
A. Gel, Y. Jiao, H. Emady, C. Tong, J. Hu and N. Ellingwood




2016 Crosscutting Research And Rare Earth Elements  
Portfolios Review, Pittsburgh, PA  
04/21/2016

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**Presentation Outline**




- The Project Team
- Technical Background/Motivation for The Project
- Potential Significance of The Results of The Work
- Physical Modeling Enhancement
- Industrial Collaboration and Utility

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**MFIX-DEM Phi team: ASU campus**



- PI: Aytekin Gel
- PhD, West Virginia U. 1999
- MBA, ASU, 2007
- Professor of Practice, School of Computing, Informatics, Decision Systems Engineering (SCIDSE), ASU
- Expertise: HPC, CFD, UQ, multiphase reactive flow, Six Sigma for Quality
- 16 years of startup company exp.
- Involved with MFIX since 1999
- Award: Team Member of R&D 100, 2007



- Co-PI: Heather Emady
- PhD, Purdue U. 2012
- Assistant Professor, School of Engineering, Materials, Transport and Energy (SEMTE)
- Expertise: particulate processes and product design
- Award: Bisgrove Scholar, 2015




- Co-PI: Yang Jiao
- PhD, Princeton U. 2010
- Assistant Professor, School of Engineering, Materials, Transport and Energy (SEMTE)
- Expertise: computational materials
- Award: DARPA Young Faculty, 2014



- GRA: Manogna Adepu
- PhD candidate, SEMTE



- GRA: Shaohua Chen
- PhD candidate, SEMTE





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**MFIX-DEM Phi Team Member at  
Lawrence Livermore National Laboratory (LLNL)**

- Co-PI: Charles Tong
- Research Scientist
- Expertise: uncertainty quantification
- Developer of open-source UQ toolbox PSUADE and CCSI Toolkit UQ framework FOQUS



**MFIX-DEM Phi Team Members at  
Sandia National Laboratory (SNL)**

- Co-PI: Jonathan Hu
- Principal Member of the Technical Staff at Sandia National Laboratories
- Expertise: highly scalable linear equation solver, developer of Trilinos Project (ML, nextgen ML: MueLu)
- Award: R&D 100 (Trilinos)



- Nathan Ellingwood
- Research Staff at Sandia National Laboratories
- Ph.D. in Applied Math & and Computational Sciences, University of Iowa (2014)
- Expertise: Data parallel algorithms for GPU, FEM, CFD, HPC, Digital Lung Project









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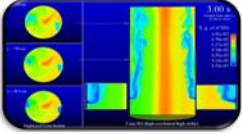
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**MFIx**  
Open Source Suite  
(<https://mfix.netl.doe.gov>)

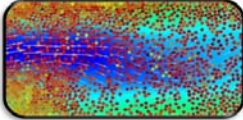
**(1) MFIx-TFM (Eulerian-Eulerian)**

	Serial	DMP	GMP
Momentum Equations	●	●	●
Energy Equations	●	●	●
Species Equations	●	●	●
Chemical Reactions	●	●	●
Cartesian cut-cell	●	●	□



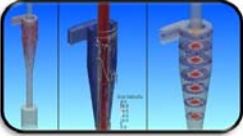
**(2) MFIx-DEM (Eulerian-Lagrangian with CFD+DEM or DEM only)**

	Serial	DMP	GMP
Momentum Equations	●	●	●
Energy Equations	●	●	●
Species Equations	●	●	●
Chemical Reactions	●	●	●
Cartesian cut-cell	○	○	○



**(3) MFIx-PIC (Eulerian-Lagrangian with Parcel in Cell)**




	Serial	DMP	GMP
Momentum Equations	●	●	○
Energy Equations	●	●	○
Species Equations	●	●	○
Chemical Reactions	●	●	○
Cartesian cut-cell	○	○	○



**(4) MFIx-Hybrid (Eulerian-Lagrangian-Eulerian blend of TFM + DEM)**

● – implemented and fully tested  
○ – implemented with limited testing  
□ – not tested or status unknown

Source: MFIx 2015-1 user guide.




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**MFIx\* Open Source Multiphase Flow Solver Suite:**  
**MFIx Two-Fluid Model (TFM) Equations Solved:**

Mass conservation for phase m (m=g for gas and s for solids)

$$\frac{\partial}{\partial t} (\epsilon_m \rho_m) + \nabla \cdot (\epsilon_m \rho_m \vec{v}_m) = \sum_{l=1}^{N_m} R_{ml}$$

Momentum conservation

$$\frac{\partial}{\partial t} (\epsilon_m \rho_m \vec{v}_m) + \nabla \cdot (\epsilon_m \rho_m \vec{v}_m \vec{v}_m) = \nabla \cdot \bar{S}_m + \epsilon_m \rho_m \vec{g} + \sum_n \bar{I}_{mn}$$

Granular energy conservation (m ≠ g)


$$\frac{3}{2} \epsilon_m \rho_m \left( \frac{\partial \Theta_m}{\partial t} + \vec{v}_m \cdot \nabla \Theta_m \right) = \nabla \cdot \bar{q}_{\Theta_m} + \bar{S}_m : \nabla \vec{v}_m - \epsilon_m \rho_m J_m + \Pi_{\Theta_m}$$

Energy conservation


$$\epsilon_m \rho_m C_{pm} \left( \frac{\partial T_m}{\partial t} + \vec{v}_m \cdot \nabla T_m \right) = -\nabla \cdot \bar{q}_m + \sum_n \gamma_{mn} (T_n - T_m) - \Delta H_{rm}$$

Species mass conservation


$$\frac{\partial}{\partial t} (\epsilon_m \rho_m X_{ml}) + \nabla \cdot (\epsilon_m \rho_m X_{ml} \vec{v}_m) = R_{ml}$$



<https://mfix.netl.doe.gov>



R&D100 Award  
2007






FLC  
Mid-Atlantic Region  
Tech-Transfer  
Award 2006

Sources:


- Syamlal et al. "MFIx Documentation, Theory Guide," DOE/METC-94/1004, NTIS/DE9400087 (1993)
- Benyahia et al. "Summary of MFIx Equations 2005-4", From URL <http://www.mfix.org/documentation/MfixEquations2005-4-3.pdf>, July 2007.

\* MFIx: **M**ultiphase **F**low with **I**nterphase **e**xchanges




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**MFIX\* Open Source Multiphase Flow Solver Suite:**  
**MFIX Discrete Element Method (DEM) Equations:**

  
<https://mfix.netl.doe.gov>

Newtonian Equations for Particles

$$\frac{d\mathbf{X}^{(i)}(t)}{dt} = \mathbf{V}^{(i)}(t),$$

$$m^{(i)} \frac{d\mathbf{V}^{(i)}(t)}{dt} = \mathbf{F}_T^{(i)} = m^{(i)} \mathbf{g} + \mathbf{F}_d^{(i \in k, m)}(t) + \mathbf{F}_c^{(i)}(t),$$

$$I^{(i)} \frac{d\boldsymbol{\omega}^{(i)}(t)}{dt} = \mathbf{T}^{(i)}$$

Particle Contact Force Models

$$\mathbf{F}_{nij}(t) = \mathbf{F}_{nij}^S(t) + \mathbf{F}_{nij}^D(t) \quad \mathbf{F}_{tij}(t) = \mathbf{F}_{tij}^S(t) + \mathbf{F}_{tij}^D(t)$$

Drag Forces on Particles

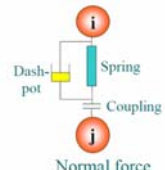
$$\mathbf{F}_d^{(i \in k, m)} = -\nabla P_g(\mathbf{x}_k) V_m + \frac{\beta_m^{(k)} V_m}{\varepsilon_{sm}} (\mathbf{v}_g(\mathbf{x}_k) - \mathbf{v}_{sm}(\mathbf{x}_k))$$

Solid-Fluid Momentum Transfer

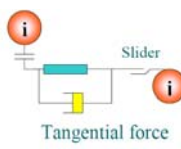
$$\mathbf{T}_{gm}^k = -\varepsilon_{sm} \nabla P_g(\mathbf{x}_k) + \beta_m^{(k)} (\mathbf{v}_g(\mathbf{x}_k) - \mathbf{v}_{sm}(\mathbf{x}_k))$$

Sources:




- R Garg, J Galvin, T Li, S Pannala, "Documentation of open-source MFIX-DEM software for gas-solids flows" (2010)



Normal force



Tangential force




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**MFIX Overview (Today)**  
*A suite of multiphase flow models & solvers*

Model Uncertainty

**PIC**

*Track parcels of particles and approximate collisions*

*Two-Fluid Model: Gas and solids form an interpenetrating continuum*

**TFM**

*Continuum and discrete solids coexist*


**Hybrid**

Trade-off between simulation fidelity and time-to-solution




*Discrete Element Method: Track individual particles and resolve collisions*

**DEM**

*Time-to-Solution*



Source: Musser et al. "MFIX Update", 2014 NETL Workshop on Multiphase Flow Science (2014)




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## MFIX: A Unified Framework and Code Base for Eulerian-Lagrangian and Lagrangian Treatment of Multiphase Flows

**Governing Equations Solved**

$$\frac{\partial(\rho_f \phi)}{\partial t} + \nabla \cdot (\rho_f \phi \mathbf{v}_f) = 0 \quad \frac{D}{Dt}(\rho_f \phi \mathbf{v}_f) = \nabla \cdot \bar{\tau}_f + \rho_f \mathbf{g} + \sum_{k=1}^K \mathbf{f}_{k,f}$$

$$\bar{\tau}_f = -p_f \bar{\mathbf{I}} + \bar{\tau}_f \quad \bar{\tau}_f = 2\mu_f \nabla \cdot \mathbf{v}_f + \lambda_f \nabla \cdot \nabla \cdot \mathbf{v}_f$$

$$\mathbf{f}_{k,f}^{(i,j)} = -\nabla \cdot (\mathbf{N}_{k,f}^{(i,j)} \mathbf{v}_f) + \frac{d(\rho_f \phi)}{dt} (\mathbf{v}_f \mathbf{N}_{k,f}^{(i,j)} - \mathbf{v}_f^{(i,j)})$$

$$\mathbf{f}_{k,s} = \frac{1}{V_k} \sum_{i \in \mathcal{N}_k} \mathbf{f}_{k,f}^{(i,j)} \mathbf{N}_{k,s}^{(i,j)} \mathbf{v}_f$$

Spring-dashpot & Hertzian contact models are implemented

$$\mathbf{f}_{k,s}^{(i,j)} = \sum_{l \in \mathcal{N}_k^{(i,j)}} \mathbf{f}_{k,s}^{(i,j,l)} + \mathbf{f}_{k,s}^{(i,j)} \quad \mathbf{f}_{k,s}^{(i,j,l)} = \sum_{m \in \mathcal{N}_k^{(i,j,l)}} (\mathbf{v}_f^{(i,j,l)} - \mathbf{v}_f^{(m)})$$

First-order integration scheme

$$\mathbf{v}_f^{(i,j)}(t + \Delta t) = \mathbf{v}_f^{(i,j)}(t) + \frac{\mathbf{f}_{k,s}^{(i,j)}(t)}{m_{k,s}} \Delta t$$

$$\mathbf{N}_{k,s}^{(i,j)}(t + \Delta t) = \mathbf{N}_{k,s}^{(i,j)}(t) + \Delta t \mathbf{f}_{k,s}^{(i,j)}(t)$$

$$\mathbf{v}_f^{(i,j)}(t + \Delta t) = \mathbf{v}_f^{(i,j)}(t) + \frac{\mathbf{f}_{k,s}^{(i,j)}(t)}{m_{k,s}} \Delta t$$

Adams-Bashforth second-order integration scheme

$$\mathbf{v}_f^{(i,j)}(t + \Delta t) = \mathbf{v}_f^{(i,j)}(t) + \frac{\Delta t}{2} (2\mathbf{f}_{k,s}^{(i,j)}(t) - \mathbf{f}_{k,s}^{(i,j)}(t - \Delta t))$$

$$\mathbf{N}_{k,s}^{(i,j)}(t + \Delta t) = \mathbf{N}_{k,s}^{(i,j)}(t) + \Delta t (\mathbf{f}_{k,s}^{(i,j)}(t) + \frac{1}{2} (\mathbf{f}_{k,s}^{(i,j)}(t) - \mathbf{f}_{k,s}^{(i,j)}(t - \Delta t)))$$

$$\mathbf{v}_f^{(i,j)}(t + \Delta t) = \mathbf{v}_f^{(i,j)}(t) + \frac{\Delta t}{2} (3\mathbf{f}_{k,s}^{(i,j)}(t) - 2\mathbf{f}_{k,s}^{(i,j)}(t - \Delta t) + \mathbf{f}_{k,s}^{(i,j)}(t - 2\Delta t))$$

No need for external coupling of multiple software as done in most of the current available options such as CFDEM® coupling by CFDEMresearch GmbH:

OpenFOAM

↑ External Coupling ↓

LIGGGHTS®

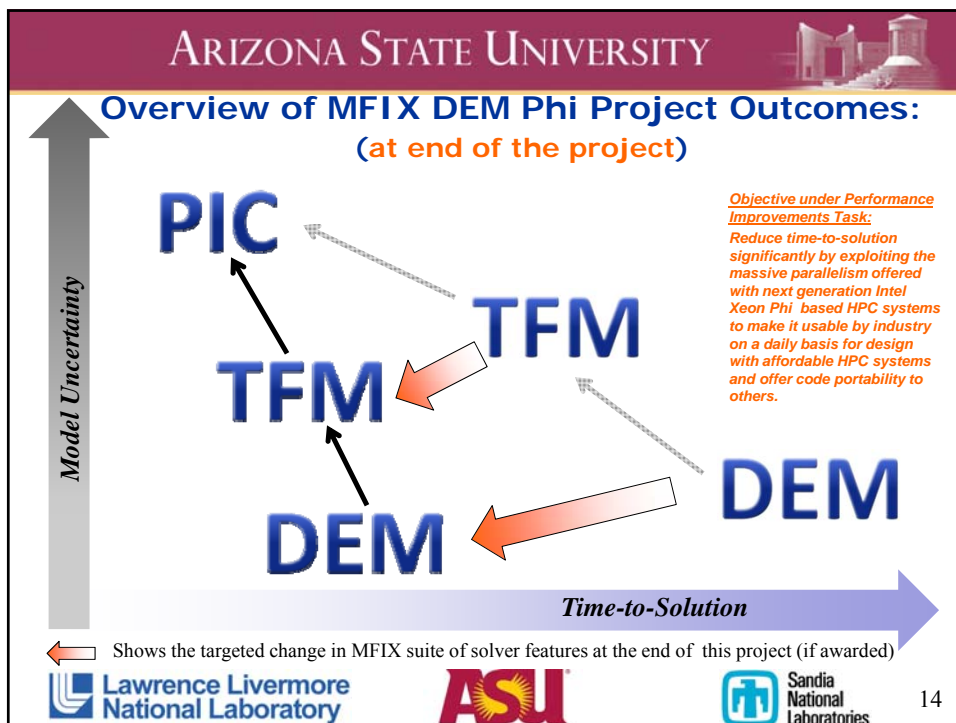
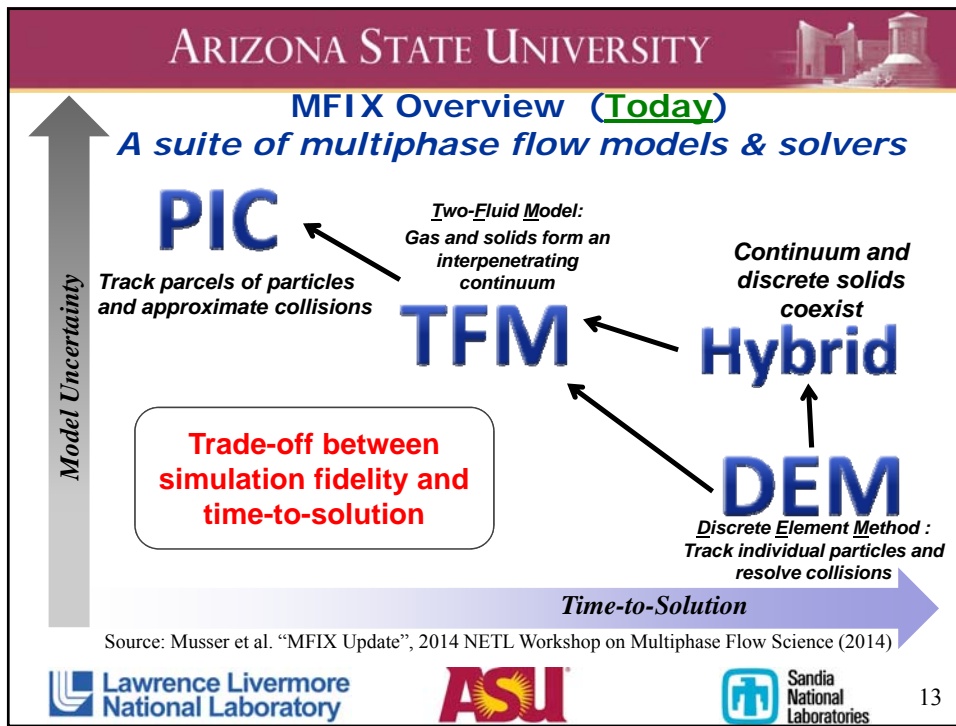
Flow chart illustrating the key solution processes coupling the CFD solver and DEM solver and the associated governing equations

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- Potential Significance of The Results of The Work
- ☐ Physical Modeling Enhancement
- ☐ Industrial Collaboration and Utility



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**MFIX-DEM Phi: Performance and Capability Improvements Towards Industrial Grade Open-source DEM Framework with Integrated Uncertainty Quantification**

**Task 2 Aim:**  
Increase the speed to reduce time-to-solution by optimizing modern computing platforms

**Task 5 Aim:**  
Demonstrate usability for industrial scale problems and collaboration for industrial adoption.

**Task 4 Aims:**  
Ensure the results of the code are accurate. Increase usability by reducing complexity

**Task 3 Aim:**  
Develop physics w.r.t. the targeted application

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- Physical Modeling Enhancement- Enhance the Capability for Handling
  - Particle Size Distributions
  - ☐ Heat Transfer
- ☐ Industrial Collaboration and Utility






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**Physical Modeling Enhancement**



## Enhance the Capability for Handling Particle Size Distributions

- New data structures have been implemented to separate geometrical and physical parameters of each particles of a solid phase, and to allow each solid phase to possess a different size distribution.
- New subroutines have been written to generate initial particle configurations with built-in distributions, including Gaussian, Log-Normal, and Uniform.
- New subroutines have been written to generate initial particle configurations with arbitrary user-defined particle size distributions.
- Subroutines using particle radii as parameters have been modified accordingly.
- The implementations have been tested in a discharging hopper case provided by one of the collaborator.

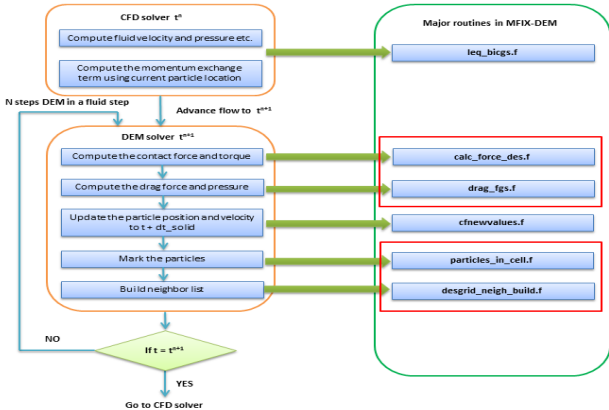



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**Physical Modeling Enhancement**

## Enhance the Capability for Handling Particle Size Distributions

### Summary of subroutine modification






```

graph TD
    subgraph CFD_solver [CFD solver t^n]
        C1[Compute fluid velocity and pressure etc.]
        C2[Compute the momentum exchange term using current particle location]
    end
    subgraph DEM_solver [DEM solver t^{n+1}]
        D1[Compute the contact force and torque]
        D2[Compute the drag force and pressure]
        D3[Update the particle position and velocity to t = dt_solid]
        D4[Mark the particles]
        D5[Build neighbor list]
    end
    subgraph MFIX_DEM [Major routines in MFIX-DEM]
        R1[leq_bigs.f]
        R2[calc_force_des.f]
        R3[drag_fgs.f]
        R4[cfnwvalues.f]
        R5[particles_in_cell.f]
        R6[desgrid_neigh_build.f]
    end
    C1 --> R1
    C2 --> R1
    D1 --> R2
    D2 --> R3
    D3 --> R4
    D4 --> R5
    D5 --> R6
    
```

**Implemented distribution types:**  
Uniform, Normal(Gaussian), LogNormal

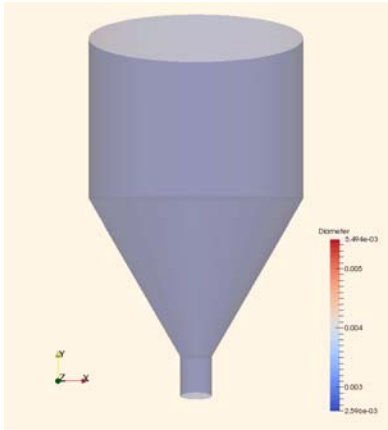
**Added commands for ICs:**  
IC\_PSD\_TYPE(ICV, Phase)  
IC\_PSD\_MEAN\_DP(ICV, Phase)  
IC\_PSD\_STDEV(ICV, Phase)  
IC\_PSD\_MAX\_DP(ICV, Phase)  
IC\_PSD\_MIN\_DP(ICV, Phase)

**Added commands for BCs:**  
BC\_PSD\_TYPE(BCV, Phase)  
BC\_PSD\_MEAN\_DP(BCV, Phase)  
BC\_PSD\_STDEV(BCV, Phase)  
BC\_PSD\_MAX\_DP(BCV, Phase)  
BC\_PSD\_MIN\_DP(BCV, Phase)

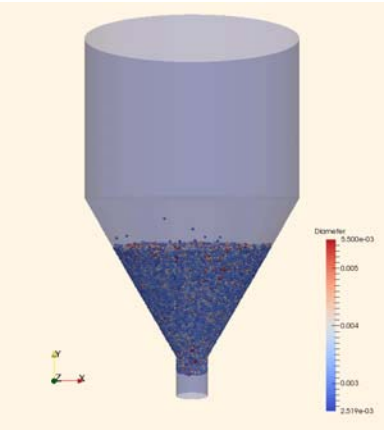



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**Enhance the Capability for Handling Particle Size Distributions – Preliminary Results for Bin Flow Case**



Particle injection (0.4s) and settling (0.3s)




Particle discharge (4.0 s)




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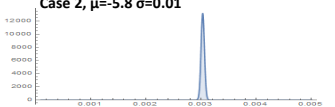
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**Enhance the Capability for Handling Particle Size Distributions**

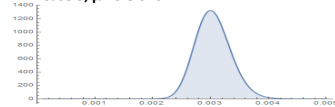
Case 1,  $\mu=5.8 \sigma=0.001$




Case 2,  $\mu=5.8 \sigma=0.01$



Case 3,  $\mu=5.8 \sigma=0.1$



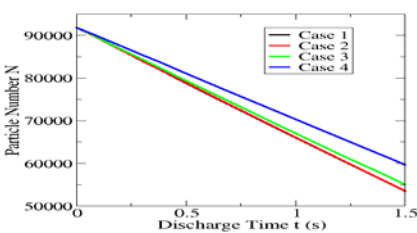
Case 4,  $\mu=5.8 \sigma=0.25$






**Packing Fraction**

	Case 1	Case 2	Case 3	Case 4
<b>MFX-DEM</b>	<b>0.605</b>	<b>0.608</b>	<b>0.624</b>	<b>0.659</b>
<b>LAMMPS</b>	<b>0.609</b>	<b>0.604</b>	<b>0.633</b>	<b>0.662</b>

**Discharge Dynamics**






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**Enhance the Capability for Handling Particle Size Distributions**

**Hopper with mass inflow BC**

Three solid phases:  
**phase 1,  $\mu=-5.3 \sigma=0.05(MI)$**   
**phase 2,  $\mu=-5.5 \sigma=0.05$**   
**phase 3,  $\mu=-5.8 \sigma=0.05$**

particle # vs. discharging time

Time (Seconds)	Particle #
0.0	68000
0.2	67500
0.4	67000
0.6	66500
0.8	66000
1.0	65500
1.2	65000
1.4	64500
1.6	64000
1.8	63500
2.0	63000

Diameter: 5.499e-03  
0.005  
0.004  
0.003  
2.504e-03

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**Enhance the Capability for Handling Particle Size Distributions**

**Cyclone**

**Log-Normal**  
 $\mu=-3.90$   
 $\sigma=0.05$




Diameter: 2.546e-02  
0.02304  
0.02093  
0.01861  
1.639e-02

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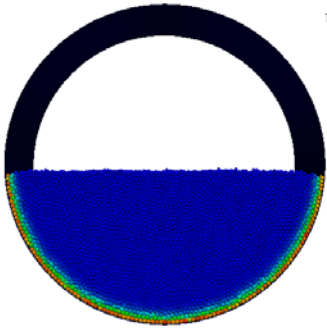
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  - ✓ Particle Size Distributions
  - Heat Transfer
- ❑ Industrial Collaboration and Utility

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Physical Modeling Enhancement



Snapshot of wall HT after 2 sec of simulation.

**Enhance the Capability for Handling Heat Transfer through experimental validation**

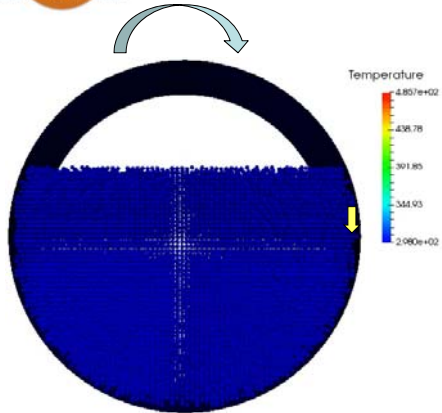
- Conduction, convection, and radiation occur in many multiphase processes. Particle-particle conduction is now commonly used in DEM codes, but more complex heat transfer models are necessary to more accurately simulate these processes.
- Current serial version of MFIX-DEM has codes for each of these, but they remain to be tested and validated.
- Whether drying, mixing, granulating, coating or heating, rotary drum systems are among the most common process equipment, offering efficient economical solutions. Thus, a rotary drum was selected for validating heat transfer models.

Source : <http://www.muzzio.rutgers.edu/>

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Physical Modeling Enhancement



Temperature  
4.857e+02  
436.76  
301.85  
344.93  
2.080e+02




**Enhance the Capability for Handling Heat Transfer through experimental validation**

- The drum is held at a fixed hot temperature of 600K with particles placed in the drum with a temperature of 300K and air at 298 K. The drum is rotated at a speed of 2 RPM in clockwise direction.
- Simulating particle-wall and particle-fluid-particle heat transfer

Animation of wall heat transfer (2 sec)

**Simulation parameters**

Diameter of drum	6 inch.
Height of drum	3 inch.
Fill Volume	50 %
Number of particles	100,000
Density of particles	1500 kg/m <sup>3</sup>
Diameter of particles	0.002 m
K_s: solid conductivity	1 W/(m-K)
Cp_s: specific heat of solid	850 J/(kg-K)
K_g: air conductivity	0.0372 W/(m-K)
Cp_g: specific heat of air	1020 J/(kg-K)




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Physical Modeling Enhancement




**Enhance the Capability for Handling Heat Transfer**

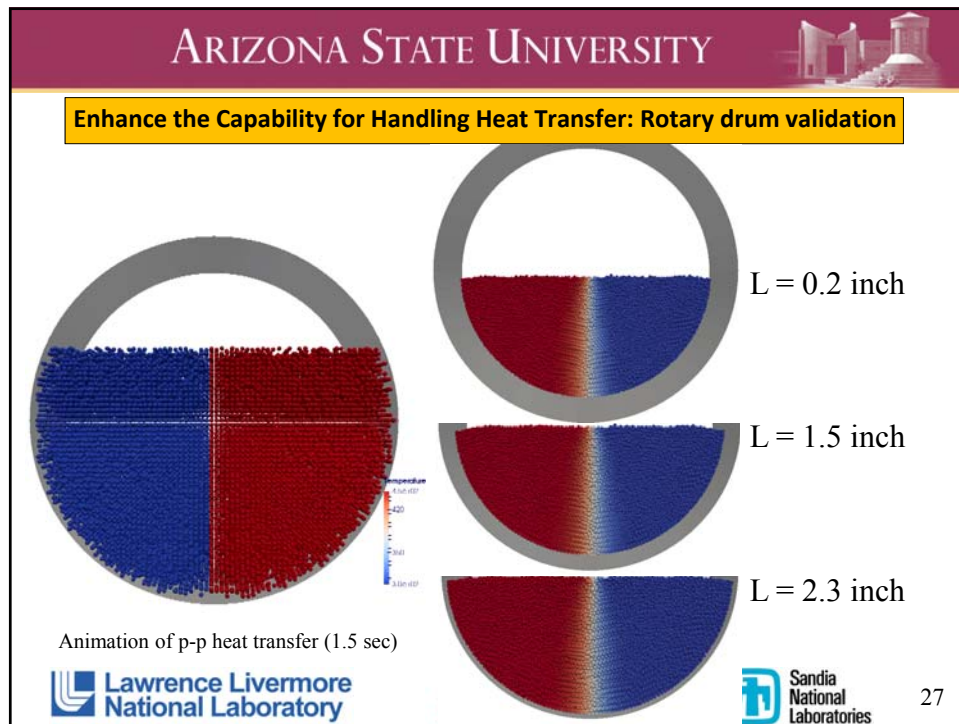
**Experimental Validation**

- A rolling aluminum calciner with thermocouples inserted in the radial direction.
- One side is Teflon and one side is glass for internal view.
- Particle - particle and particle - wall conduction has been validated in this paper.
- Further fluid-particle convection and radiation via particle-environment modes will be tested and validated.

Source: Bodhisattwa Chaudhuri, et al. "Experimentally validated computations of heat transfer in granular materials in rotary calciners". Powder Technology 198 (2010) 6-15.

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Lawrence Livermore National Laboratory

**ASU**

Sandia National Laboratories

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Industrial  
Collaboration  
& Utility


**Perform Industry Outreach and Development of Industry Cases**




- FOA Objectives requires demonstration of the new capabilities with at least one industrially relevant problem.
- For a demonstration of the process to continually obtaining industry feedback was stated.
- From the beginning of this project, we teamed up with two major industrial collaborators with distinctly different application domains:

World's largest publicly traded international oil and gas company:




One of the largest global consumer goods company:



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Industrial  
Collaboration  
& Utility

**Perform Industry Outreach and Development of Industry Cases**




**Test Case # 1 provided by one of the Industrial Collaborator :**

- Bin Flow (Hopper settling and discharge): A cylindrical hopper was initially filled with a set of spherical particles which were allowed to settle under the influence of gravity. The bottom of the hopper was then opened and the material was allowed to pour from the hopper. We track the flow rate of material from the hopper as a comparison metric case, which they use as a granular flow benchmarking test case for assessing various CFD software. Also input deck for LIGGGHTS (open-source DEM code) to facilitate comparative assessment.



	Model 1
Initial # of particles	300 000
Particle diameter (m)	0.003
Particle density (kg/m <sup>3</sup> )	1000
Poisson ratio	0.25
Young's modulus (MPa)	25
Coefficient of restitution	0.5
Static friction coefficient	0.2
Rolling friction coefficient	0.0
Timestep (sec)	10 <sup>-6</sup>
Settling time (sec)	1.5
Flow time (sec)	3.0

Model parameters for bin flow simulations.

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Industrial Collaboration & Utility

**Perform Industry Outreach and Development of Industry Cases**

**Test Case # 1 provided by Industrial Collaborator: Preliminary Results**

Results from	cores	Particles after 1.5 s	% reduction in particles	
MFIX 2015-2 release version	MPI only	16	262,552	-12.50 %
LIGGGHTS (as per collaborator runs)	MPI only	20	257,997	-14.00%

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Industrial Collaboration & Utility

**Perform Industry Outreach and Development of Industry Cases**


**Validation of hopper discharge rate and pure granular flow**

Experimental setup of the scaled down hopper


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**Perform Industry Outreach and Development of Industry Cases**




**Validation of hopper discharge rate and pure granular flow**  
**Hopper discharge using sand**





**Experimental Parameters**

Hopper height	10 cm
Fill height	8 cm
Total time	1.2 min
Wt. of sand	193.4 gm
Size range	[0.064 0.174] mm

- Sand was used to demonstrate the experimental setup and working.
- Once the setup is finalized silica beads will be used for validating the granular flow.







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The overarching goal is for MFI<sub>X</sub>-DEM to be able to solve industrial-scale problems, and to encourage its adoption by industry.







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**Overall goal of the project**

- ❖ Lowering the barrier for industrial users and researcher in adopting MFIX in day-to-day use.
  - Physical modelling enhancements to capture the physics more accurately and reduce uncertainty.
  - Performance Improvements to reduce time-to-solution by taking advantage of current and next generation HPC system which will be available and affordable.
  - Integrated uncertainty quantification that is easy to use.




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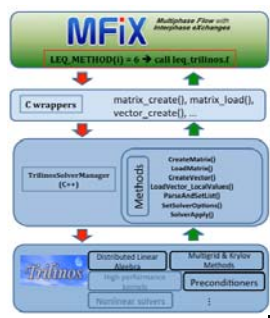



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## Questions?

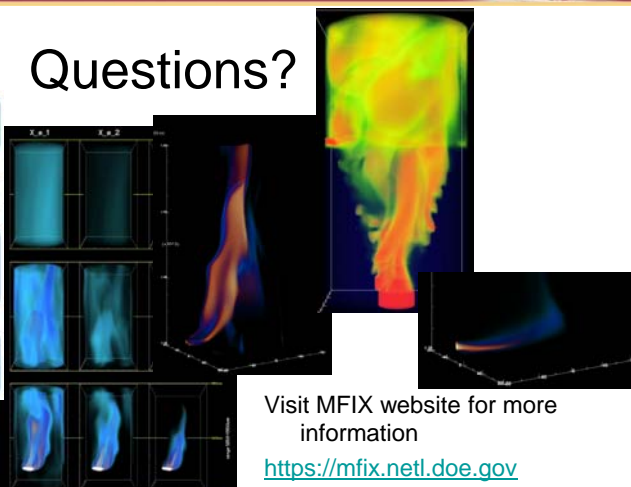


**MFIX** Multiphase Flow with  
Multiphase Exchanges  
LEQ\_METHOD() -> call leg\_trilinos.f

**C wrappers**  
matrix\_create(), matrix\_load(),  
vector\_create(), ...




**TrilinosSolverManager (C++)**  
Methods:  
CreateMatrix(),  
LoadMatrix(),  
CreateVector(),  
LoadVector\_LocalValues(),  
Parallelize(),  
SetSolverOptions(),  
SolveByPhys()

**Trilinos**  
Distributed Linear Algebra, Multigrid & Krylov Methods, High performance preconditioners, Nonlinear solvers, ...



Visit MFIX website for more information  
<https://mfix.netl.doe.gov>

Source: Visualizations prepared by A. Gel & OLCF Visualization Support for Commercial Scale Gasifier Simulations with MFIX as part of INCITE award (2010)  
<https://mfix.netl.doe.gov/results.php#commercialscalegasifier>

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### Performance and Capability Improvements



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**Performance Improvement**

Physical Modeling Enhancement

Integrated Uncertainty Quantification





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Performance Improvement  **Background:**


- Currently supercomputing capability on a desktop possible, if you can make your program to run efficiently on it!


Many in Core (MIC) from Intel ,  
First generation Intel Xeon Phi (named Knights Corner):

- **Approximately 1 TeraFLOP/s** computing capability for double precision (1<sup>st</sup> generation)

Graphical Processing Unit (GPU) from NVIDIA:

- **Approximately 3 TeraFLOP/s** computing capability for double precision







**TFLOP/s**= Trilinos floating point operations per second






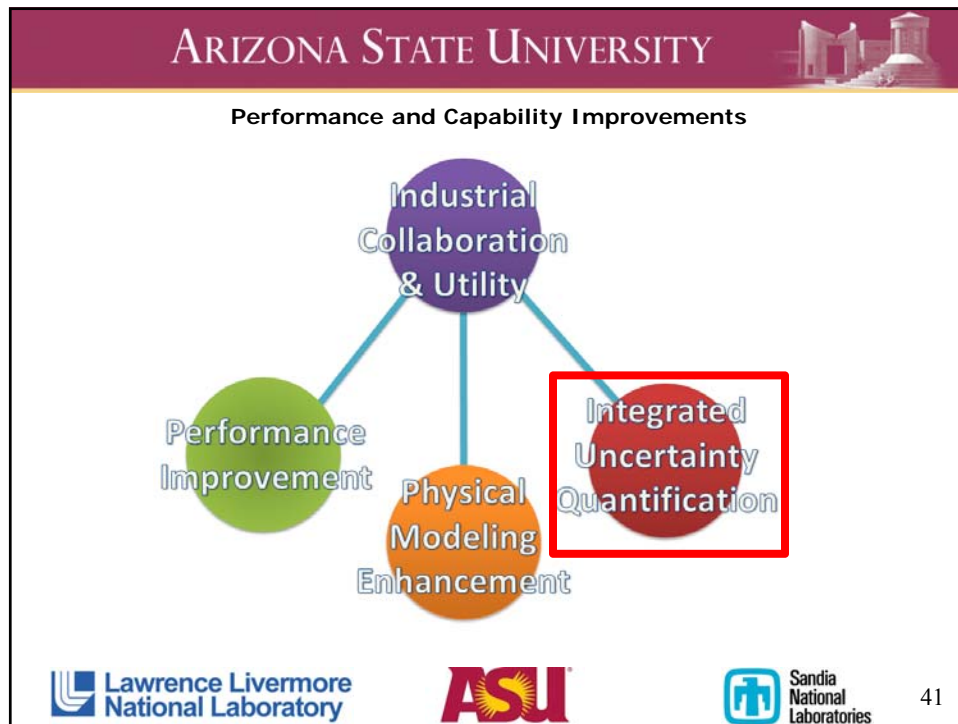

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Performance Improvement  **Proposed Methodology & Solution:**

- Legacy CFD software still in demand
  - Due to extensive validation performed.
- However, require code modernization to take advantage of new HPC platforms:
  1. **Bottom-up approach:** Hot-spot guided code refactoring and optimization
  2. **Top-down approach:** Leverage external scalable solvers from Trilinos Project




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Integrated  
Uncertainty  
Quantification

## Background:

- An increasing interest in the assessment of predictive credibility of simulation and computational modeling.
- Several barriers exist in the effective use of practical computational models in the engineering design process by industry:
  - Lack of user-friendly tools to perform critical analyses like uncertainty quantification
  - Lack of adequate background in statistical sciences
- Increasing computational power and parallelism offers a unique capability of performing non-intrusive UQ.

Lawrence Livermore National Laboratory ASU Sandia National Laboratories

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